

## IN THE CLAIMS

Claims 1-10 (Cancelled)

Claim 11 (Currently Amended) A process for hydrocarbon conversion, adsorption or separation, in the presence of the SAPO-34 crystalline molecular sieve ~~of claim 1~~ manufactured by a process comprising the steps of: (a) forming a surfactant-free synthesis mixture containing sources of silicon, of aluminium, and of phosphorus, in proportions appropriate to the formation of SAPO-34, and a structure-directing agent, where the source of silicon is a tetraalkyl orthosilicate, and (b) subjecting the synthesis mixture to hydrothermal treatment.

Claim 12 (Currently Amended) A process for the conversion of an oxygenate to olefins in the presence of the SAPO-34 crystalline molecular sieve ~~of claim 1~~ manufactured by a process comprising the steps of: (a) forming a surfactant-free synthesis mixture containing sources of silicon, of aluminium, and of phosphorus, in proportions appropriate to the formation of SAPO-34, and a structure-directing agent, where the source of silicon is a tetraalkyl orthosilicate, and (b) subjecting the synthesis mixture to hydrothermal treatment.

Claim 13 (Original) A process for the conversion of an oxygenate to olefins in a reactor, the process comprising the steps of (a) contacting the oxygenate under catalytic conversion conditions with a SAPO-34 molecular sieve having a mean particle size of at most 400 nm; and (b) withdrawing olefins from the reactor.

Claim 14 (Cancelled)

Claim 15 (Cancelled)

Claim 16 (Cancelled)

Claim 17 (New) The process of claim 11 wherein the molar ratio of silicon to aluminium, expressed as  $\text{SiO}_2 : \text{Al}_2\text{O}_3$ , is at most 0.5:1.

Claim 18 (New) The process of claim 11 wherein the tetraalkyl orthosilicate is a tetraethyl orthosilicate.

Claim 19 (New) The process of claim 11 wherein the tetraalkyl orthosilicate is selected from the group consisting of a tetramethyl orthosilicate, a tetrapropyl orthosilicate, and a tetrabutyl orthosilicate.

Claim 20 (New) The process of claim 11 wherein the structure-directing agent is TEAOH or a mixture of TEAOH and DPA.

Claim 21 (New) The process of claim 11 wherein at least a part of the hydrothermal treatment step is carried out with agitation.

Claim 22 (New) The process of claim 11, wherein the synthesis mixture has a molar composition within the ranges of

$\text{P}_2\text{O}_5$	:	$\text{Al}_2\text{O}_3$	0.6 to 1.2:1
$\text{SiO}_2$	:	$\text{Al}_2\text{O}_3$	0.01 to 0.5:1
$\text{H}_2\text{O}$	:	$\text{Al}_2\text{O}_3$	10 to 100:1

together with the structure-directing agent.

Claim 23 (New) The process of claim 11 wherein the synthesis mixture is surfactant-free.

Claim 24 (New) The process of claim 11 wherein the SAPO-34 crystalline molecular sieve has a mean particle size of at most 400 nm.

Claim 25 (New) The process of claim 11 wherein the SAPO-34 crystalline molecular sieve has a mean particle size of at most 200 nm.

Claim 26 (New) The process of claim 11 wherein the SAPO-34 crystalline molecular sieve has a mean particle size of at most 100 nm.

Claim 27 (New) The process of claim 11 wherein the SAPO-34 crystalline molecular sieve is subjected to the step(s) of one or more of the group consisting of washing, cation exchange, and calcining.